

Amendments to the Specification:

Please replace paragraph [0095] with the following amended paragraph:

[0095] A full scale plant operating the CANSOLV[®] System DeSO_x process was designed to process 11,000 Nm³/h of gas at a temperature of $\leq 65^{\circ}\text{C}$. The absorbent was a diamine solvent sold under the trade mark ~~Cansolv Absorbent DS~~ CANSOLV ABSORBENT DS[™] absorbent and the unit was operated at the following conditions: lean amine flow of 10 to 13 m³/hr at an amine concentration of about 25% wt; stripper pressure of about 0.1 bar gauge. The feed gas design SO₂ content was 40.9 g/Nm³. The plant was operated over a range of gas flows, SO₂ contents and at a range of HSS levels. Figure 3 shows a plot of concentration of SO₂ in the treated gas vs. the HSS level and also the steam usage vs. HSS. As is evident from the linear regression trend lines shown in Figure 3, as the HSS level increases, both the steam requirement and the SO₂ concentration in the treated gas decrease quite remarkably.

Please replace paragraph [0099] with the following amended paragraph:

[0099] A pilot unit with a feed gas capacity of about 100 Nm³/h was used. The absorbent was ~~Cansolv[®] Absorbent DM~~ CANSOLV ABSORBENT DM[™] absorbent and the unit was operated at the following conditions: feed gas SO₂ content about 9% volume, scrubber temperature about 50°C and amine concentration of 20 - 30% by weight.